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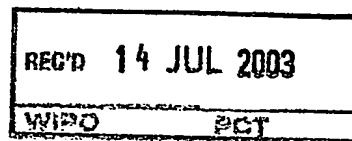
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the documents annexed hereto are true copies of:

Application forms P.1 and P.3, provisional specification and drawing  
of South African Patent Application No. 2002/4641 as originally  
filed in the Republic of South Africa on 10 June 2002 in the name  
of RUSSIL TECHNOLOGIES CC for an invention entitled: " DENSIFYING OF  
A BULK PARTICULATE MATERIAL".

Geteken te  
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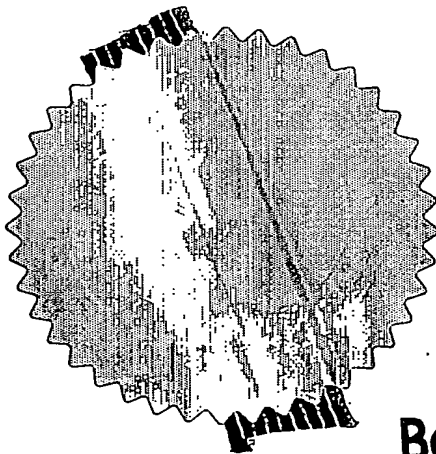
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REPUBLIC OF SOUTH AFRICA  
PATENTS ACT, 1978  
APPLICATION FOR A PATENT AND  
ACKNOWLEDGEMENT OF RECEIPT  
(Section 30(1) Regulation 22)

FORM P.1  
(to be lodged in duplicate)

REPUBLIC OF SOUTH AFRICA  
PATENT OFFICE

10.6.02

R 060.00

THE GRANT OF A PATENT IS HEREBY REQUESTED BY THE UNDERMENTIONED APPLICANT  
ON THE BASIS OF THE PRESENT APPLICATION FILED IN DUPLICATE

21 01 PATENT APPLICATION NO. 2002/4641

A&A REF. 15249370

71 FULL NAME(S) OF APPLICANT(S)

RUSSIL TECHNOLOGIES CC

ADDRESS(ES) OF APPLICANT(S)

1 Delft Street, Die Heuwel, Witbank, 1035, Republic of South Africa

54 TITLE OF INVENTION

DENSIFYING OF A BULK PARTICULATE MATERIAL

Only the items marked with an "X" in the blocks below are applicable.

☐ THE APPLICANT CLAIMS PRIORITY AS SET OUT ON THE ACCOMPANYING FORM P.2. The earliest priority claimed is

Country: No:

Date:

☐ THE APPLICATION IS FOR A PATENT OF ADDITION TO PATENT APPLICATION NO. 21 01

☐ THIS APPLICATION IS A FRESH APPLICATION IN TERMS OF SECTION 37 AND BASED ON  
APPLICATION NO. 21 01

THIS APPLICATION IS ACCOMPANIED BY:

- ☒ A single copy of a provisional specification of 14 pages  
☒ Drawings of 4 sheets  
☐ Publication particulars and abstract (Form P.8 in duplicate) (for complete only)  
☐ A copy of Figure of the drawings (if any) for the abstract (for complete only)  
☐ An assignment of invention  
☐ Certified priority document(s). (State quantity)  
☐ Translation of the priority document(s)  
☐ An assignment of priority rights  
☐ A copy of Form P.2 and the specification of RSA Patent Application No. 21 01  
☒ Form P.2 in duplicate  
☐ A declaration and power of attorney on Form P.3  
☐ Request for ante-dating on Form P.4  
☐ Request for classification on Form P.9  
☐ Request for delay of acceptance on Form P.4  
☐ Extra copy of informal drawings (for complete only)

74 ADDRESS FOR SERVICE: Adams & Adams, Pretoria

Dated this 10TH day of JUNE 2002

ADAMS & ADAMS  
APPLICANTS PATENT ATTORNEYS

The duplicate will be returned to the applicant's address for service as  
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REPUBLIC OF SOUTH AFRICA  
PATENTS ACT, 1978  
DECLARATION AND POWER OF ATTORNEY  
(Section 30 - Regulation 8, 22(i)(c) and 33)

PATENT APPLICATION NO		
21	01	2002/4641

A&A Ref: V15249

LODGING DATE	
22	10 JUNE 2002

FULL NAME(S) OF APPLICANT(S)	
71	RUSSEL TECHNOLOGIES CC

FULL NAME(S) OF INVENTOR(S)	
72	RUSSEL-SMITH, Kevan Vaughan

EARLIEST PRIORITY CLAIMED	COUNTRY	NUMBER	DATE
	33	NIL	31
		NIL	32
			NIL

NOTE: The country must be indicated by its International Abbreviation - see schedule 4 of the Regulations

TITLE OF INVENTION	
54	DENSIFYING OF A BULK PARTICULATE MATERIAL

I/we **RUSSEL-SMITH, Kevan Vaughan**

hereby declare that :-

1. ~~I/we am/are the applicant(s) mentioned above;~~
2. ~~I/we have been authorized by the applicant(s) to make this declaration and have knowledge of the facts herein stated in the capacity of~~ **MEMBER** ~~of the applicant(s);~~
3. ~~the inventor(s) of the abovementioned invention is/are the person(s) named above and the applicant(s) has/have acquired the right to apply by virtue of an assignment from the inventor(s);~~
4. ~~to the best of my/our knowledge and belief, if a patent is granted on the application, there will be no lawful ground for the revocation of the patent;~~
5. ~~this is a convention application and the earliest application from which priority is claimed as set out above is the first application in a convention country in respect of the invention claimed in any of the claims; and~~
6. the partners and qualified staff of the firm of ADAMS & ADAMS, patent attorneys, are authorised, jointly and severally, with powers of substitution and revocation, to represent the applicant(s) in this application and to be the address for service of the applicant(s) while the application is pending and after a patent has been granted on the application.

SIGNED THIS 6TH DAY OF DECEMBER 2002

Company Name: **RUSSEL TECHNOLOGIES CC**  
Full Names: **RUSSEL-SMITH, Kevan Vaughan**  
Capacity: **MEMBER**

(no legalization necessary)

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- \*\* If the applicant is a natural person, delete paragraph 2.
- \*\*\* If the right to apply is not by virtue of an assignment from the inventor(s), delete "an assignment from the inventor(s)" and give details of acquisition of right.
- \*\*\*\* For non-convention applications, delete paragraph 5.

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REPUBLIC OF SOUTH AFRICA  
Patents Act, 1978

**PROVISIONAL SPECIFICATION**  
(Section 30 (1) - Regulation 27)

21	01	OFFICIAL APPLICATION NO
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22	LODGING DATE
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10 JUNE 2002

2002/4641

71	FULL NAME(S) OF APPLICANT(S)
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RUSIL TECHNOLOGIES CC

72	FULL NAME(S) OF INVENTOR(S)
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RUSSEL-SMITH, Kevan Vaughan

54	TITLE OF INVENTION
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DENSIFYING OF A BULK PARTICULATE MATERIAL

THIS INVENTION relates to densifying of a bulk particulate material. In particular, it relates to a method and to apparatus for densifying a bulk particulate material.

5 According to one aspect of the invention, there is provided a method of densifying a bulk particulate material to provide a densified flowable bulk particulate material, the method including mechanically agitating the bulk particulate material in the presence of a densification agent thereby to provide a flowable bulk particulate material of increased bulk density.

0 The densification agent will typically be a liquid, although it is not excluded from the scope of the invention that the densification agent may be a gas or a vapour, or even another particulate material. It is however a feature of the invention that it is not necessary to remove the densification agent after having densified the bulk particulate material. The densification agent is thus used in quantities small enough to ensure that the densified bulk particulate material remains flowable and  
15 does not form a slurry. The quantity of densification agent used is also so small that the mere presence of the densification agent in the bulk particulate material does not materially alter the bulk density of the combined particulate material and the densification agent. This bulk density is only materially changed by severely agitating the combined particulate material and the densification agent, without any significant  
20 agglomeration of the particulate material.

The densification agent may be a polar liquid. In a preferred embodiment of the invention, the densification agent is an aqueous liquid, e.g. water or demineralised water.

When the densification agent is an aqueous liquid, the bulk particulate material may include water in a mass concentration falling in a range with a lower limit of about 0.5 %. The lower limit may however be as low as about 0.45 %, or even as low as about 0.4 %. An upper limit of the range may be as high as about 10 %, or even higher at about 15 %, or even as high as about 20 %.

It is however to be appreciated that the bulk particulate material being densified may affect the effective range within which an aqueous densification agent can be used. The aforementioned ranges are however suitable for the densification of microsilica, such as silica fume.

The bulk particulate material may be a hygroscopic material. The bulk particulate material may be microsilica, e.g. fumed silica, precipitated silica, colloidal silica or silica gel. The bulk particulate material may be selected from the group consisting of carbon black, fly ash, kaolin and meta kaolin. The bulk particulate material may be  $Mn_2O_3$ ,  $Mn_3O_4$ ,  $V_2O_5$  or cement or slag.

When the bulk particulate material is particulate silica, the particulate silica may have a particle size of the less than  $0.5 \mu m$ , typically less than  $0.2 \mu m$ . Indeed, it is expected that the invention will find particular, though not exclusive application in densifying so-called silica fume.

The method may include adding the densification agent to the bulk particulate material, prior to or during mechanical agitation of the bulk particulate material.

Mechanically agitating the bulk particulate material in the presence of the densification agent may include at least partially confining the bulk particulate material and rotating a rotatable member submerged under the bulk particulate material about an axis of rotation to cause severe agitation of the material. Typically, when the densification agent is present, the severe agitation of the bulk particulate material does not cause significant fluidisation of the bulk particulate material.

Mechanically agitating the bulk particulate material in the presence of the densification agent may include severely agitating the bulk particulate material with a rotatable member submerged in the bulk particulate material in a vessel and rotating about an axis of rotation which is upwardly extending, and inhibiting displacement of material downwardly past the rotating member during rotation of the rotatable member whilst allowing free movement of materials in the vessel above the rotating member.

The bulk particulate material may be confined in a vessel having a closed bottom, the rotatable member being located immediately above the bottom of the vessel.

The rotatable member may define at least one material contacting surface facing substantially tangentially in the direction of rotation thereby to cause movement of material particles essentially towards or away from the axis of rotation at least on initial contact of the material particles with the material contacting surface. A radially outer end of the material contacting surface may lead a radially inner end thereof.

The material contacting surface is thus typically slanted, i.e. non-perpendicular or non-radial to the direction of rotation to cause material particles to move tangentially and/or radially relative to the axis of rotation. One or more radially extending material contacting surfaces, or surfaces of variable orientation, e.g. defined by flexible members, are however not excluded from the scope of the invention.

In one embodiment of the invention, the rotatable member defines a plurality of circumferentially spaced material contacting surfaces each facing substantially tangentially in the direction of rotation with a radially outer end of the surface leading a radially inner end thereof. Each material contacting surface may be defined by a slanted vane.

The rotatable member may thus include a plurality of circumferentially spaced vanes projecting from an upper surface of a disc-shaped body, the disc-shaped body and the vessel which confines the bulk particulate material cooperating to inhibit axial displacement of the agitated bulk particulate material downwardly past the rotating member during rotation of the rotatable member. Instead, the vanes may project tangentially or radially outwardly from a periphery of the disc-shaped body or from a hub.

Each vane may define a planar material contacting surface extending upwardly parallel to the axis of rotation of the rotatable member.

The rotatable member may be rotated such that a point on an extreme radially outer periphery of the rotatable member, submerged in the bulk particulate material, travels at a speed of between about 5 m/s and about 80 m/s, typically between about 21 m/s and about 23 m/s.

Confining the bulk particulate material may include feeding the bulk particulate material into a vessel. Thus, an entire body of bulk particulate material may be densified inside the vessel to provide a uniform body of particulate material having a uniform bulk density inside the vessel. Typically, the vessel has a wall defining a circular cylindrical interior surface or a cone-shaped interior surface. The vessel may have a central, longitudinal axis which is coaxial with the axis of rotation of the rotatable member.



The method may include vibrating the vessel to inhibit agglomeration or build-up or caking of the particulate material against interior surfaces of the vessel.

The method may include discharging the flowable densified bulk particulate material from the vessel. It is to be appreciated that the method can be conducted on a continuous basis or on a batch basis, discharging of the densified bulk particulate material from the vessel and feeding of bulk particulate material into the vessel thus occurring batch-wise, or on a controlled basis. Thus, the bulk particulate material may be fed on a continuous basis into the vessel, and the densified bulk particulate material may be discharged on a continuous basis from the vessel, the entire body of bulk particulate material inside the vessel having, at steady state conditions, a substantially higher bulk density than bulk particulate material feed.

The method may include measuring or determining the bulk density of the densified bulk particulate material prior to discharging it from the vessel. Instead, the method may include measuring or determining the bulk density of the densified bulk particulate material after it has been discharged from the vessel.

The method may include controlling the density of the densified bulk particulate material. The controlling of the density of the densified bulk particulate material may be effected by a method selected from the group consisting of manipulating the residence time of the bulk particulate material in the vessel, manipulating the angular speed of rotation of the rotatable member, manipulating the level of the bulk particulate material in the vessel, controlling the concentration of the densification agent present with the bulk particulate material, and two or more of these methods. The controlling of the density of the densified bulk particulate material is however not necessarily limited to these methods.

The axis of rotation of the rotatable member may be substantially vertical. In another embodiment of the invention, the coaxial axis of rotation and longitudinal axis of the vessel are at an angle of about  $60^\circ$  to the horizontal.

The rotatable member may be rotated at an angular speed of between 100 rpm and 3500 rpm. Preferably, the rotatable member is rotated at an angular speed of between 500 rpm and 1000 rpm. Typically, the rotatable member is rotated at an angular speed of between 700 rpm and 800 rpm, e.g. about 732 rpm.

5 The bulk particulate material may have a mean particle size of less than 1 mm. Typically, the bulk particulate material has a mean particle size of less than 0.5 mm, even less than 1  $\mu\text{m}$ , e.g. about 0.15  $\mu\text{m}$ .

The method may include extracting dust from the vessel.

0 The ratio of the bulk density of the particulate material prior to densifying thereof, to the bulk density of the flowable densified particulate material may be at least 2 : 3. Preferably, the ratio of the bulk density of the particulate material prior to densifying thereof, to the bulk density of the flowable densified particulate material is at least 1 : 5, depending on the bulk density of the particulate material prior to densifying and the particulate material being densified. The ratio can be as large as  
5 1 : 10, or even larger, e.g. 1 : 12 depending on the bulk density of the particulate material prior to densifying and the particulate material being densified.

According to another aspect of the invention, there is provided bulk particulate material densification apparatus which includes  
a vessel for at least partially confining a body of the bulk particulate material;  
20 a rotatable member which is arranged such that in use it is submerged in the body of bulk particulate material mechanically to agitate the bulk particulate material;  
a densification agent inlet leading into the vessel; and  
drive means connected to the rotatable member and capable of rotating the  
rotatable member about said axis of rotation when the rotatable member is submerged  
25 in the body of bulk particulate material.

The rotatable member may be as hereinbefore described.

When the rotatable member includes a plurality of vanes, a radially inner end portion of at least some of the vanes may be truncated so that the radially inner end of the vane forms an angle of between  $15^\circ$  and  $60^\circ$  with the axis of rotation in the plane of the vane. Preferably, the angle is between  $20^\circ$  and  $50^\circ$ , e.g. about  $30^\circ$ .

The vessel may have an outlet for densified bulk particulate material at a low elevation, and an inlet for bulk particulate material at a higher elevation than the outlet. Preferably, the rotatable member is located at the elevation of the outlet of the vessel.

The drive means may be capable of rotating the rotatable member at an angular speed of between 100 rpm and 3500 rpm when the rotatable member is submerged in the body of particulate material. Typically, the drive means is capable of rotating the rotatable member at an angular speed of between 500 rpm and 1000 rpm when the rotatable member is submerged in the body of particulate material, e.g. at about 700 rpm to 800 rpm.

The vessel may have a wall defining a circular cylindrical interior surface or a conical interior surface, and a central, longitudinal axis which may be coaxial with the axis of rotation of the rotatable member. The ratio of the diameter of a circle described by the rotatable member when it rotates, to the diameter of the vessel may be between 0.25 : 1 and 0.99 : 1. Preferably, the ratio is at least between 0.5 : 1 and 0.99 : 1. Typically, the ratio of the diameter of the circle described by the rotatable member when it rotates, to the diameter of the vessel is at least between 0.9 : 1 and 0.99 : 1, e.g. about 0.95 : 1.

The vessel may have a volume of between  $0.1 \text{ m}^3$  and  $200 \text{ m}^3$ . Typically, the vessel has a volume of between  $0.1 \text{ m}^3$  and  $0.5 \text{ m}^3$ .

The axis of rotation of the rotatable member may be substantially vertical.

The apparatus may include conveying means and bagging means, the conveying means being arranged to convey densified bulk particulate material from the vessel to the bagging means for bagging the densified bulk particulate material.

The apparatus may include vibration means for vibrating the vessel to inhibit agglomeration or caking or build-up of the particulate material against interior surfaces of the vessel.

The apparatus may include dust extraction means for extracting dust from the vessel.

The rotatable member and interior surfaces of the vessel may be coated with a material which inhibits caking or agglomeration or build-up of the bulk particulate material against or on them.

The apparatus may include density measurement means and control means for controlling the bulk density of the densified bulk particulate material.

The invention will now be described, by way of example, with reference to the accompanying diagrammatic drawings and examples.

In the drawings

Figure 1 shows a sectioned elevational view of one embodiment of densification apparatus in accordance with the invention for densifying a bulk particulate material;

Figure 2 shows a three-dimensional view of a rotatable member of the densification apparatus of Figure 1;

Figure 3 shows a sectioned elevational view of another embodiment of densification apparatus in accordance with the invention for densifying a bulk particulate material; and

Figure 4 shows a three-dimensional view of a rotatable member of the densification apparatus of Figure 3.

Referring to Figure 1 of the drawings, reference numeral 10 generally indicates one embodiment of densification apparatus in accordance with the invention for densifying a bulk particulate material. The apparatus 10 includes a vessel 12 for containing and confining the bulk particulate material, and a rotatable member 14 which is in use submerged in the bulk particulate material contained in the vessel 12, and which is rotatable about a vertical axis of rotation 16.

The vessel 12 includes a circular cylindrical wall 18 which defines a circular cylindrical interior surface 20 of the vessel 12. Thus, the vessel 12 has a central, longitudinal vertical axis which corresponds or which is coaxial with the axis of rotation 16. In another embodiment of the invention, the axis of the vessel and the axis of rotation may be angularly disposed relative to the horizon, e.g. at an angle of about 60 °.

The vessel 12 includes an inlet 22 for the bulk particulate material, and an outlet 24 for densified bulk particulate material. The inlet 22 is located in a roof 26 of the vessel 12, and the outlet 24 is located in the wall 18 of the vessel 12.

The rotatable member 14 is located at the elevation of the outlet 24. The rotatable member 14 is mechanically attached to a drive shaft 30, which is in turn drivingly connected to an electric motor (not shown). The electric motor is capable of selectively rotating the rotatable member 14 at an angular speed of between 700 rpm and 800 rpm.

The rotatable member 14 includes a disc-like body 32 from which a plurality of circumferentially spaced planar vanes 34 projects (see Figure 2). The vanes 34 are directed or arranged in use to displace the bulk particulate material contained in the vessel 12 inwardly towards the axis of rotation 16 when the body 32 is rotated slowly. The vanes 34 project from a surface 36 of the disc-like body 32 which is an operative upper surface.

The disc-like body 32, and thus the rotatable member 14, has a diameter of 720 mm. The vessel 12 has an internal diameter of about 800 mm. Thus, a ratio of the diameter of the rotatable member 14 : the diameter of the vessel 12 is 0.9 : 1.

The drive shaft 30 extends through the roof 26 of the vessel 12. A seal 38 is provided between the drive shaft 30 and the roof 26.

A conveyor belt 40 is provided underneath the vessel 12. An automatic, controlled outlet cover 60 is provided to open or close the outlet 24. A chute 62 provides flow communication between the outlet 24 and the conveyor belt 40.

A densification agent inlet 64 is provided in the wall 18, at a relatively high elevation. The inlet 64 is in flow communication with a water feed line 66. A flow controller 68 is provided in the flow line 66.

A dust extraction outlet (not shown) is provided for the vessel 12, and a vibrator (not shown) is mounted against the exterior surface of the wall 18.

In use, the vessel 12 is fed on a controlled and measured basis with bulk particulate material 44, as shown by arrow 42, to maintain a level 46 of the bulk particulate material in the vessel 12 sufficient to cover the rotatable member 14. Water is added in a predetermined controlled ratio through the inlet 64 to the bulk particulate material. When the material is silica fume, this ratio is about 3 : 100 on a mass basis.

The submerged rotatable member 14 is rotated at an angular speed of about 732 rpm, in the direction of arrow 48, by means of the electric motor and the drive shaft 30. The vanes 34 severely agitate the bulk particulate material and densify the bulk particulate material. The vibrator is run to inhibit caking of the bulk particulate material against interior surfaces of the vessel 12, and dust which is formed is extracted through the dust extraction outlet.

The densified bulk particulate material is discharged through the outlet 24 and the chute 62 on to the conveyor belt 40, which moves in the direction of arrow 52. The density of the densified bulk particulate material on the conveyor belt 40 is measured by density measurement and control means (not shown), which increases or decreases the discharge rate of the densified bulk particulate material from the vessel 12 by opening or closing the outlet cover 60, thereby increasing or decreasing the residence time of the bulk particulate material in the vessel 12, in order to densify the bulk particulate material to a desired bulk density.

Referring to Figure 3 of the drawings, another embodiment of densification apparatus in accordance with the invention for densifying a bulk particulate material is generally indicated by reference numeral 100. The apparatus 100 is similar to the apparatus 10, and unless otherwise indicated, the same reference numerals used in relation to the apparatus 10, are used to indicate the same or similar parts or features of the apparatus 100.

The apparatus 100 includes a rotatable member 102, which is more clearly illustrated in Figure 4 of the drawings. As can be seen in Figure 4, the vanes 34 are vertical and planar, and are substantially tangential to the drive shaft 30 (not shown) in Figure 4, which is operatively connected to the rotatable member 102. An inner end portion of each vane 34 is truncated so that the radially inner end 35 of each vane 34 forms an angle of about 30° with the axis of rotation of the rotatable member 34, in the plane of the vane 34.

The rotatable member 102 is located at the elevation of the outlet 24 of the vessel 12. The outlet 24 is provided in a lower portion of the wall 18 of the vessel 12. A manually operated outlet cover 104 is provided to open or close the outlet 24.

The drive shaft 30 is rotatably mounted to a support member 31 by means of two plummer blocks 33 and is operatively connected to an electric motor 106, by means of a drive belt 108 and two pulleys 110, 112. The arrangement of the

motor 106 and the pulleys 110, 112 is such that, in use, the motor 106 is capable of rotating the rotatable member 102 at an average speed of between 700 rpm and 800 rpm.

The vessel 12 and motor 106 are mounted on a support structure 114.

The vessel 12 has an internal diameter of about 576mm, and a height of about 1500 mm. The rotatable member 102 has a diameter of about 550 mm. Thus, the ratio of the diameter of the rotatable member 102 to the diameter of the vessel 12 is about 0.95 : 1.

The densification agent inlet 64 is in flow communication with a funnel 120, via a gooseneck 122.

The apparatus 100 is used in similar fashion to the apparatus 10 to densify bulk particulate material, but works on a batch basis. Thus, a measured weight of bulk particulate material is fed into the vessel 12 through the inlet 22 to provide a level of the bulk particulate material in the vessel 12 sufficient to cover the rotatable member 102. A measured amount of water as densification agent is poured into the funnel 120 and allowed to flow into the vessel 12. The rotatable member 102 is rotated at an angular speed of about 732 rpm by means of the electric motor 106 and drive shaft 30. The vanes 34 severely agitate the bulk particulate material and densify the bulk particulate material. The densified bulk particulate material is discharged on a batch basis through the outlet 24 onto the conveyor belt 40 by means of a chute 116. The conveyor 40 conveys the densified bulk particulate material to a bagging plant (not shown), which bags the densified bulk particulate material.

### EXAMPLE 1

Silica fume, having a bulk density of  $100 \text{ kg/m}^3$ , was densified by means of the apparatus 100 of Figure 3, without adding water as a densification agent to the



bulk particulate material inside the vessel 12. The apparatus 100 managed to increase the bulk density of the silica fume to about  $450 \text{ kg/m}^3$ . A small quantity of water, in a ratio of about 3 : 100 on a weight basis, was added to the partially densified silica fume and the rotatable member 102 was again rotated at about 732 rpm for a short period of time. During this period, the bulk density of the silica fume inside the vessel 12 increased from about  $450 \text{ kg/m}^3$  to about  $1200 \text{ kg/m}^3$ . At the end of this period, the silica fume was still in the form of a flowable powder.

### EXAMPLE 2

The same process as described for Example 1 was used to densify carbon black. Initially, the carbon black had a bulk density of between  $40 \text{ kg/m}^3$  and  $80 \text{ kg/m}^3$ . After having partially densified the carbon black in the absence of a densification agent, the bulk density of the carbon black increased to about  $200 \text{ kg/m}^3$ . A small quantity of water (about 3 % by weight) was added to the carbon black, whereafter the carbon black was further densified to a bulk density of about  $600 \text{ kg/m}^3$  by severely agitating the carbon black by means of the rotatable member 102.

It is an advantage of the invention, as illustrated, that it provides a cost effective method and apparatus for densifying a bulk particulate material, such as silica fume. It is a further advantage of the invention, as illustrated, that the method and apparatus are capable of densifying materials such as silica fume to a higher bulk density than conventional methods and apparatus used for the densifying of silica fume and like materials.

DATED THIS 10<sup>TH</sup> DAY OF JUNE 2002



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APPLICANT'S PATENT ATTORNEYS

2002/401

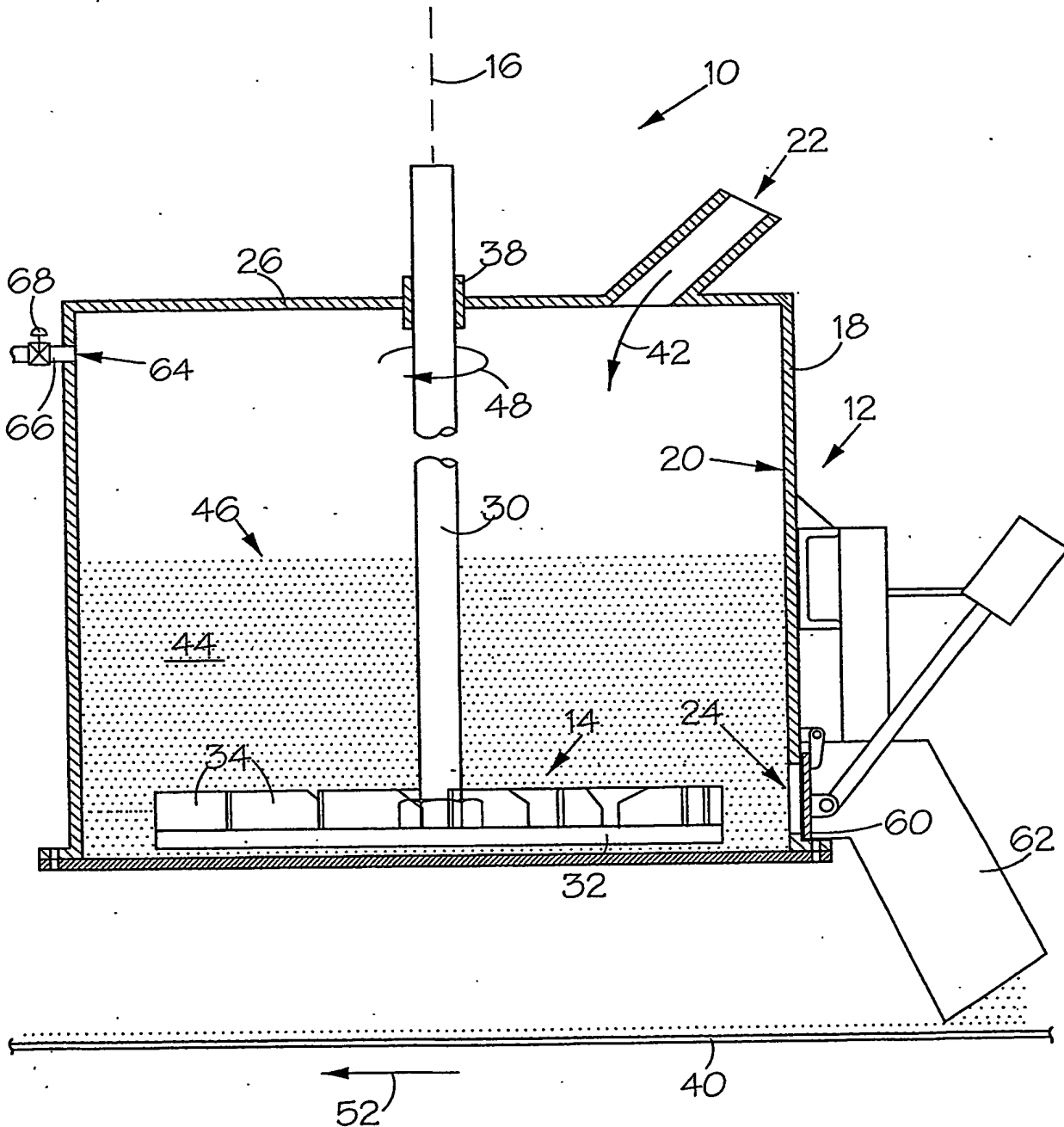


FIG 1

2002/464

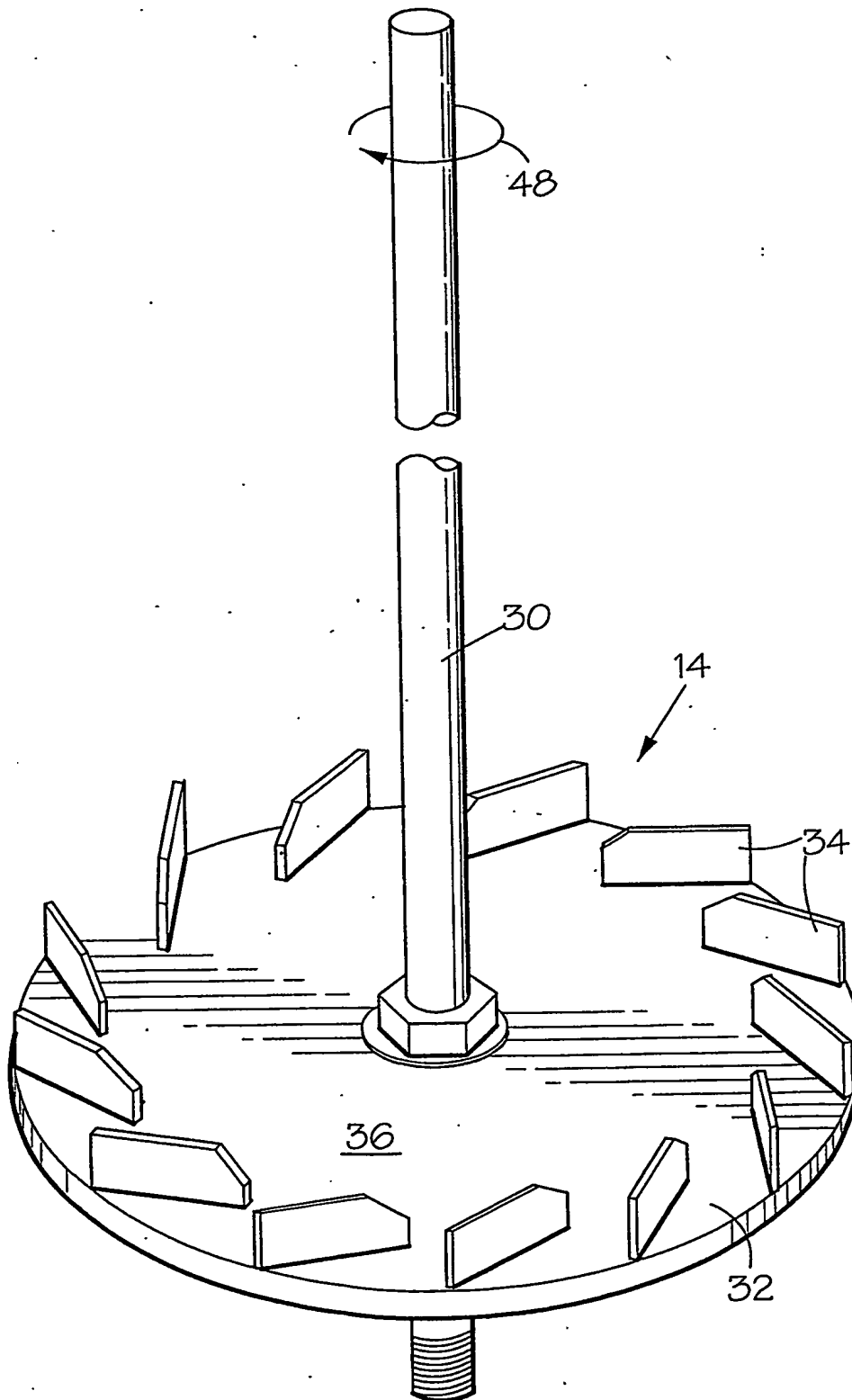


FIG 2

2002/46

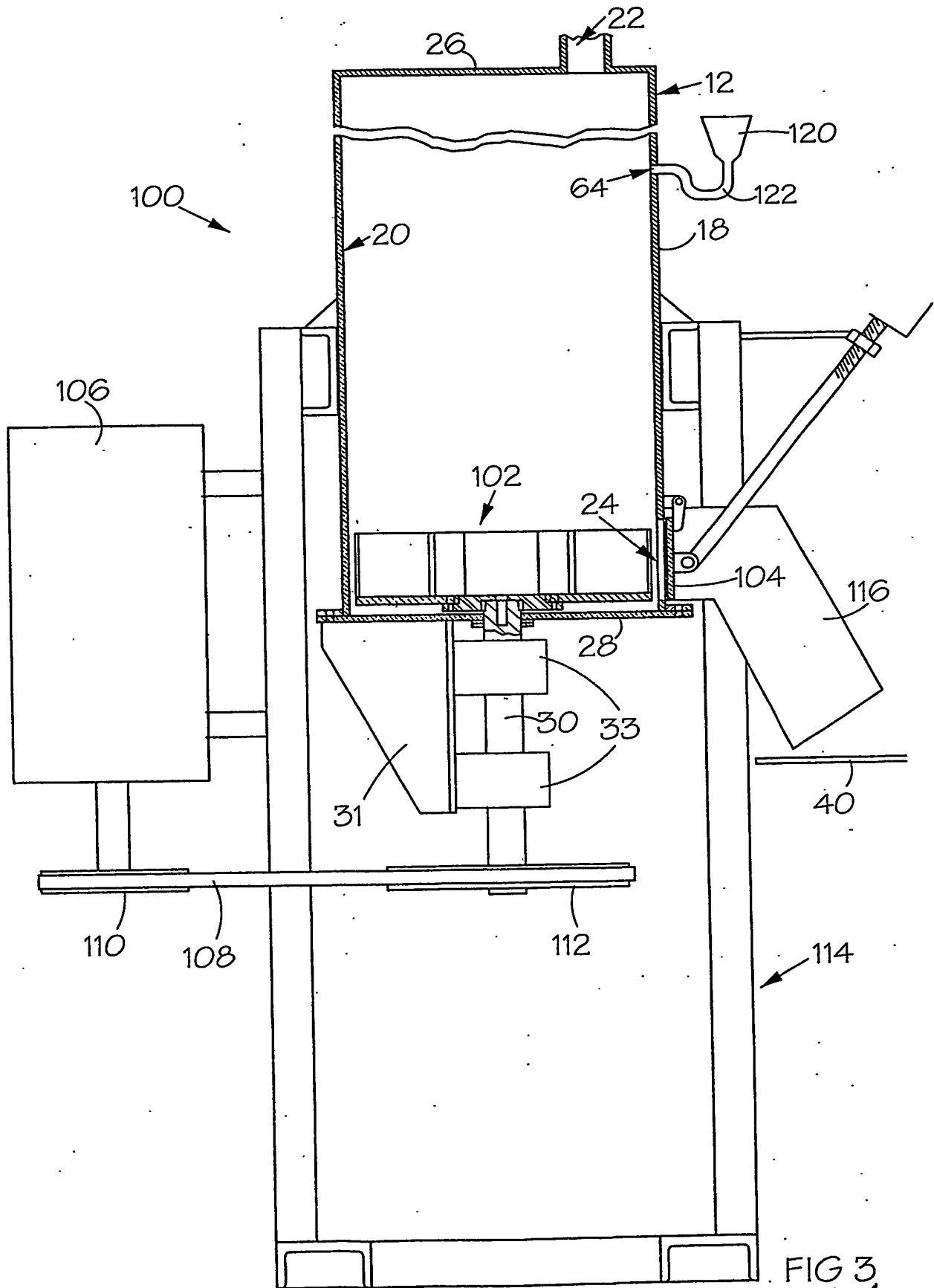
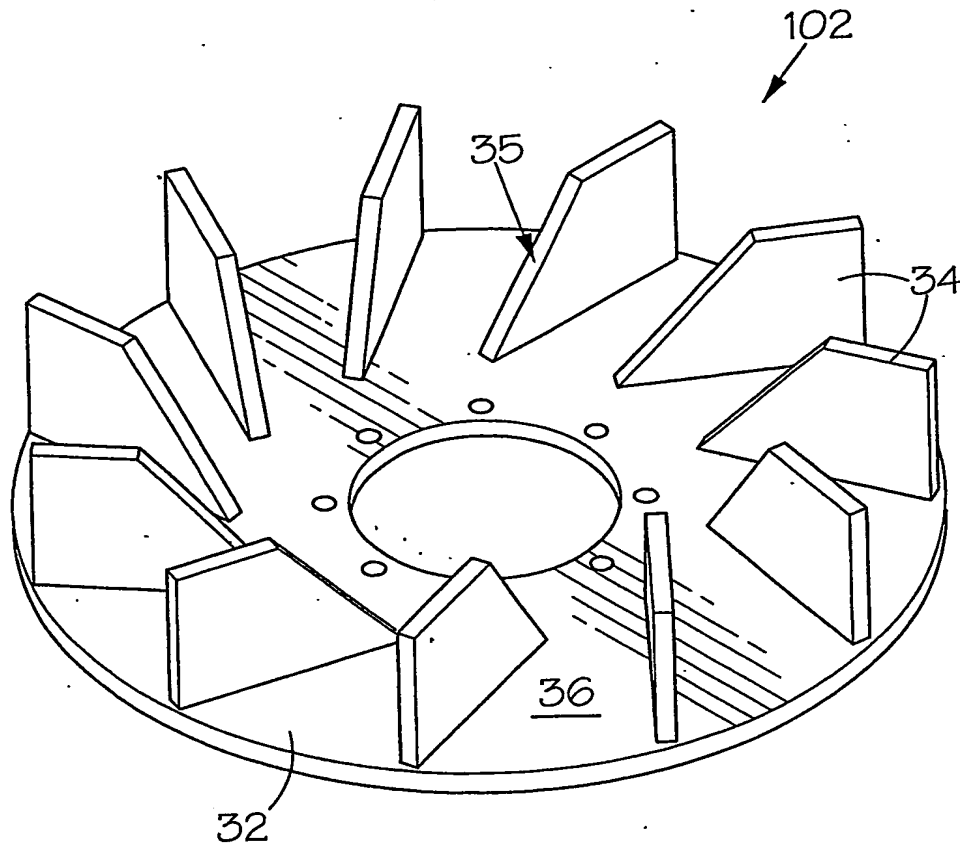


FIG 3

2002/4041



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